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DOI:

[10.3390/en14092665](https://doi.org/10.3390/en14092665)

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Document Version

Publisher's PDF, also known as Version of record

Citation for published version (Harvard):

Shamoushaki, M, Niknam, PH, Talluri, L, Manfrida, G & Fiaschi, D 2021, 'Development of cost correlations for the economic assessment of power plant equipment', *Energies*, vol. 14, no. 9, 2665. <https://doi.org/10.3390/en14092665>

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Article

Development of Cost Correlations for the Economic Assessment of Power Plant Equipment

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Abstract: A comprehensive cost correlation analysis was conducted based on available cost correlations, and new equipment cost correlation models were proposed based on QUESTOR modeling. Cost correlations for various types of equipment such as pumps, compressors, heat exchangers, air coolers, and pressure vessels were generated on the basis of extracted cost data. The models were derived on the basis of robust multivariable regression with the aim of minimizing the residuals by using the genetic algorithm. The proposed compressor models for both centrifugal and reciprocating types showed that the Turton cost estimation for carbon steel compressor and Matche's and Mhhe's data were compatible with the generated model. According to the results, the cost trend in the Turton correlation for carbon steel had a somewhat lower estimation than these correlations. Further, the cost trend of the Turton correlation for carbon steel pressure vessels was close to the presented model trend for both bullet and sphere types. The Turton cost trend for U-tube shell-and-tube heat exchangers with carbon steel shell and stainless steel tube was close to the proposed heat exchanger model. Furthermore, the Turton cost trend for the flat-plate heat exchanger using carbon steel was similar to the proposed model with a slight difference.

Keywords: cost correlation; power plant equipment; economic analysis



Citation: Shamoushaki, M.; Niknam, P.H.; Talluri, L.; Manfrida, G.; Fiaschi, D. Development of Cost Correlations for the Economic Assessment of Power Plant Equipment. *Energies* **2021**, *14*, 2665. <https://doi.org/10.3390/en14092665>

Academic Editor: Ron Zevenhoven

Received: 17 March 2021

Accepted: 28 April 2021

Published: 6 May 2021

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1. Introduction

The increasing demand for energy in many countries in recent years has fueled growth in the construction of new power plants based on conventional fuels and renewable energies. Global energy demand will rise 1.4 times, from 19,562 TWh in 2012 to 26,761 TWh by 2025, principally in the developing countries [1]. By 2025, it is expected that world power capacity will grow by a factor of 1.4, from 6117 GW in 2014 to 8370 GW to meet this growth in demand. Developing countries are expected to account for about 70% of this capacity enhancement [1].

In the recent decade, many researchers have turned particular attention to the economic assessment of various energy systems. The zonal and nodal models have been applied to evaluate the energy market. To improve and develop models based on ecological and social challenges, some suggestions have been presented by Borowski [2] to improve zonal and nodal models that may hold promise as new models for the functioning of the electricity market in Europe in the near future. Poyrazoglu [3] applied three clustering methods to pricing zone detection for an electricity market in a Turkey case study. However, a more accurate estimation of equipment costs is essential to power plants' exergo-economic analysis, as those costs have direct and influential impacts on final economic results. This importance can even affect project feasibility. To calculate power plant equipment costs, some graphs and correlations in references are available; however, most are not recent, affecting the economic analysis. Moreover, manufacturers and companies rarely share their product costs; these reasons make the economic analysis

more challenging for researchers. Applicable cost estimations have a significant impact on the profitability of a project and the technical solutions.

Capital cost estimations for a power plant are a significant element in construction decisions. In the design step, it is hard to evaluate the exact value of equipment and capital costs. There may be some scatter cost value for each unit of equipment mainly because of differences in the manufacturing process, material quality, applied technologies, the local tax, relevant expenses, etc. Material type can directly affect equipment costs, as stainless steel is around four times more expensive than steel based on MEPS International information [4].

Other researchers' economic analyses show that different approaches have been applied to the investigation of power plant investment expenses. Many researchers have used cost correlations to evaluate the equipment costs and then evaluate power plant total costs according to the calculated equipment costs. Some researchers apply the thermo-economic approach to evaluate energy systems such as combinations of the geothermal, Organic Rankine cycle (ORC), and solar technologies [5–7]. They have combined exergy and economic concepts and used the exergo-economic approach to assess certain energy cycles such as the geothermal and ORC combined cycle [8,9], gas turbine (GT) cycle [10,11], combined solid oxide fuel cell (SOFC) and GT cycle [12,13], and refrigeration cycle [14] from both the technical and economic points of view. The application of various cost estimation methods leads to different results and can affect project arrangements.

Statistical approaches can rely on correlations or alternative methods to connect equipment features to costs. Other researchers apply a regression approach or optimization methods to obtain the best cost estimation tools [15,16]. The parametric cost model related to statistical methods and criteria can be applied to determine the casual links and correlate equipment costs to develop a function with one or more dependent variables [17].

Williams [18] estimated heat exchanger costs by comparing equipment pieces of the same model. Pikulik and Diaz [19] proposed a heat exchanger cost estimation approach based on diameter, type, and nuzzle size. Purohit [20] generated a complex cost model for heat exchanger cost estimation based on many factors such as shell inner diameter, material, type, pressure, number of tube passes, tube outer diameter, tube pitch, etc. Vataavuk [21] developed a model according to 1995 data on heat exchanger area to calculate the heat exchanger costs. Wang [22] carried out a computer simulation study to derive factor-based cost correlations for a given project. According to the ICARUS process evaluator, Loh et al. [23] presented a report about the cost curves for various equipment. Their proposed purchasing equipment cost estimation was based on the capacity variable. Taal et al. [24] provided a summary of some cost estimation methods for heat exchanger equipment in the industry.

Max et al. [25] performed equipment sizing and cost estimations for process equipment based on computer aided design and optimization. They considered 10 different methods in cost evaluation. Kim et al. [26] offered an applicable cost estimating model based on the hybrid concept for large building projects comprising multiple mixed-use buildings. Yang [27] proposed a generic method to combine correlations between cost factors within the cost estimation process. The presented method checks correlation feasibility first to see if it needs any adjustment or not. Turton et al. [28] proposed cost correlations of various chemical process devices based on different equipment types, materials, and pressure ranges. Caputo and Pelagagge [29] compared parametric function and artificial neural networks to calculate the cost of large and complex-shaped pressure vessels. Ogayar and Vidal [30] developed a series of correlations to estimate the cost of a small hydro-power plant's electro-mechanical equipment using basic parameters such as power and head.

Kim, K.J., and Kim, K. [31] presented a primary cost estimation model using genetic algorithm (GA) and case-based reasoning (CBR). Feng and Rangaiah [32] compared five capital cost estimation programs for some equipment. They evaluated seven case studies related to petroleum refining, petrochemical, and biopharmaceutical processes. Towler and Sinnott [33] generated an exponential correlation form to estimate purchasing equipment

costs. Ereev and Patel [34] extended a methodology to the economic evaluation of total manufacturing production expenses by applying factors according to equipment purchase costs. Gunduz and Sahin [35] expanded two cost estimation models to evaluate hydroelectric power plant project costs by applying neural networks and multiple regression assessment in the early project stages. Symister [36] carried out capital cost estimations for chemical processing using Aspen capital cost estimator for several equipment types in his thesis. Caputo et al. [37] expanded an analytical-generative cost estimation procedure by developing a mathematical model for shell and tube heat exchangers. Luyben [38] provided a simple method to estimate compressor costs using Aspen. However, he did not apply an optimization method. Malhan and Mittal [39] applied a polynomial regression model base to generate cost correlations for the major components in micro hydro power plants. Shamoushaki et al. [40] proposed well drilling cost models for different regions. They applied robust multivariable regression to minimize the residuals. Islam et al. [41] employed an integrated fuzzy set theory and fuzzy Bayesian belief network model to risk-induced contingency cost modeling for power plant projects.

In this study, the cost analysis of the main equipment in a power plant was evaluated by extracting cost data from QUE\$TOR software based on a 2020 database [42]. The considered equipment included the pump, compressor, heat exchanger, air cooler, and pressure vessel. The process modeling was performed in QUE\$TOR, and by changing the main operational parameters of the system and equipment, relevant cost data were extracted. The curve multivariable robust regression was applied to develop equipment cost correlations comparable with data in the literature. We endeavored to generate correlations that showed the best compatibility with available data. A comprehensive cost correlation evaluation was performed on the basis of correlations presented in different research papers and references. The most reliable cost correlations were determined by comparing the proposed models with other cost correlations and data. These cost results were based on the 2020 database for the QUE\$TOR software, which suggests that they are very reliable for use by researchers and stakeholders and can help operators and investors with their decisions and estimates. This study sought to fill the gap in equipment cost estimation with these updated models.

2. Methodology and Curve Fitting

The best-fitted models were generated using curve fitting to compare with the available database. The goal of the curve fitting process was to find a function ($f(x_i, y_i)$) based on the input data, in which i is the data number. The most compatible and reliable fit was derived by minimizing the objective function defined in terms of the distance between the derived correlation and variables [43]. Generally, some innovative solutions such as the industry 4.0 paradigm, machine learning, etc., are used to develop more profitable projects in the energy market [44]. The cost data were collected based on the equipment and process modeling simulation by IHS Markit QUE\$TOR software, which used a comprehensive database (updated in 2020, Q1). We sought to extract cost data by changing the main operational parameters of the equipment and evaluating their impacts on equipment cost. A general correlation form was generated for all cases as Equation (1):

$$C = \log(x) + a.(x)^2 + b.x + c \quad (1)$$

In Equation (1), a , b , and c are constant coefficients, x is a dependent variable that can vary based on the equipment, and C is the cost (\$). A logarithmic and non-linear equation was considered on the basis of available data and cost trends; a logarithmic form is common for equipment cost estimation [31].

Several cost correlation forms were evaluated to find the best compatibility with the available data. Different fitting approaches and types were applied and considered using the reference data. Both graphical and numerical fittings were evaluated for each case to reduce errors. The examination was performed according to the residuals and statistical factors, including the fit statistics and confidence intervals on the fitted coefficients. The

former showed how much fitting was matched with the data, and the latter showed the exactitude of the coefficients. The main statistical parameters, such as sum of squares (SSE) (due to error) and coefficient of determination (R^2) were considered in the cost model evaluations. Moreover, the R-square value was evaluated for each correlation, which was a statistical parameter of how close the data was to the fitted regression line. These examinations could be performed by differentiating, integrating, interpolating, or extrapolating the fitting. In the curve fitting process, based on data dissemination and points, the fitting weight was adjusted to achieve the best compatibility with the data. Some statistical parameters of cost models were introduced in Table 1. In this table, unit A is the area of the heat exchanger.

Table 1. The statistical parameters of modeling.

Equipment	Type	Range	Number of Data	Mean (\$)	Median (\$)	Confidence Interval (%)
Compressor	Centrifugal	10–10,000 (kW)	160	3.62×10^6	3.245×10^6	± 10.5
Compressor	Reciprocating	10–10,000 (kW)	160	3.484×10^6	3.12×10^6	± 10.3
Condenser	Air cooler	1–3500 (A)	200	7.981×10^5	2.748×10^6	± 10.6
Pump	Centrifugal	20–3500 (kW)	140	6.571×10^5	6.415×10^5	± 9.4
Pressure vessel	Bullet	1–1000 (m ³)	180	3.607×10^5	2.865×10^5	± 12.1
Pressure vessel	Sphere	1–1000 (m ³)	180	4.994×10^5	3.95×10^5	± 12.4
Heat exchanger	Shell & Tube	1–3500 (A)	200	7.048×10^5	2.259×10^6	± 10.2
Heat exchanger	Flat plate	1–1000 (A)	180	5.439×10^5	2.761×10^5	± 9.1

Considering the objective function according to Equation (2), independent error minimization was performed [45] by the genetic algorithm, which is a heuristic approach based on natural selection. It was utilized to optimize the correlations and derive the relevant coefficients [46].

$$\text{Min} : \sum_{j=1}^m \sum_i^n \left((x_{i,j} - x'_{i,j})^2 \right) \quad (2)$$

In this equation, $x_{i,j}$ and $x'_{i,j}$ are calculated as reference values, respectively. There is no restriction of correlation form and coefficient number in this minimization method [45]. The upper limit of iteration was considered to be 2000. The selected population was different for each piece of equipment, and the generation was considered 300. Additionally, the mutation and crossover fraction factors were supposed to be 0.2 and 0.8, respectively. The genetic algorithm was chosen because of its specific advantages: acceptable convergence rate, suitability for a wide variety of optimization problems, wide solution space searchability, and ease in discovering global optimums and avoiding trapping in local optimal. The genetic algorithm does not require any information about the function's structure to be optimized and uses it as a Black Box. Despite being proposed almost 50 years ago, the genetic algorithm, due to its performance, is still an exciting tool in various fields. It can be seen that this algorithm remains a handy tool in finance and economics, and particularly in forecasting the prices of various commodities [47].

After generating the cost model for each piece of equipment, other cost correlations and data based on the available correlation from different references were compared with the proposed model to find the most reliable correlations. As the costs based on various correlations reveal scattered results, finding the most fitted and general correlations to reach the exact evaluation of total plant cost is crucial. Comprehensive cost correlations were collected and are listed in Appendix A, which contains cost correlations for pumps, heat exchangers, condensers, and compressors. As the inflation rate directly impacts equipment costs, the inflation rate index should be applied in the economic assessment

process. The Chemical Engineering Plant Cost Index (CEPCI) was applied based on the year of each equation presented to consider the current year's inflation rate. The related cost correlation based on the Turton correlations [28] was considered in the examination process. Besides these, other available cost data from other websites (Matche [48] and Mhhe [49]) and references were collected to compare with the proposed cost models. The schematic diagram of the fitted line for the centrifugal compressor is displayed in Figure 1. This graph shows that the proposed model had a good fitting with available cost data. The flowchart of cost model generation is illustrated in Figure 2. The schematic of a conventional geothermal power plant with target equipment for this study is illustrated in Figure 3.

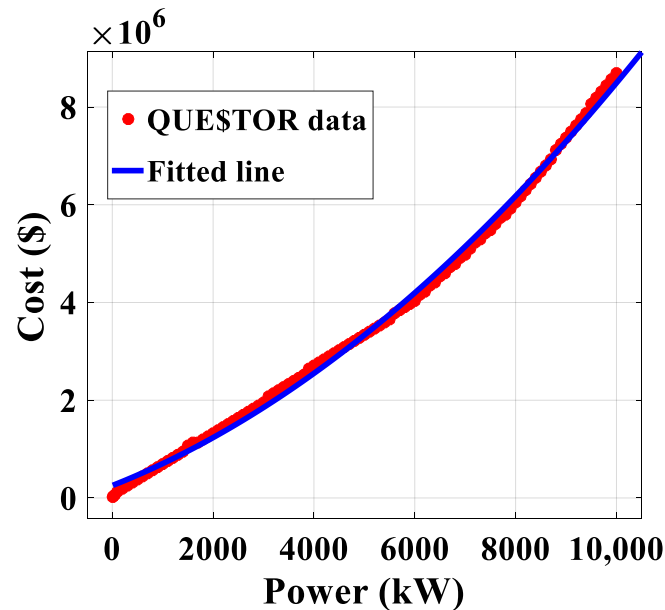


Figure 1. Fitting line for centrifugal compressor.

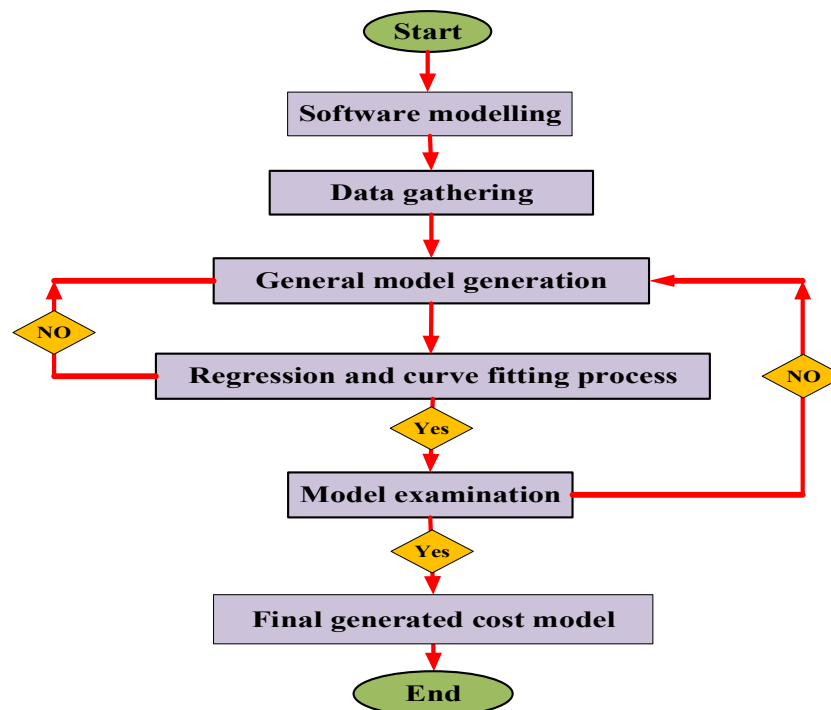


Figure 2. Flowchart of cost model generation.

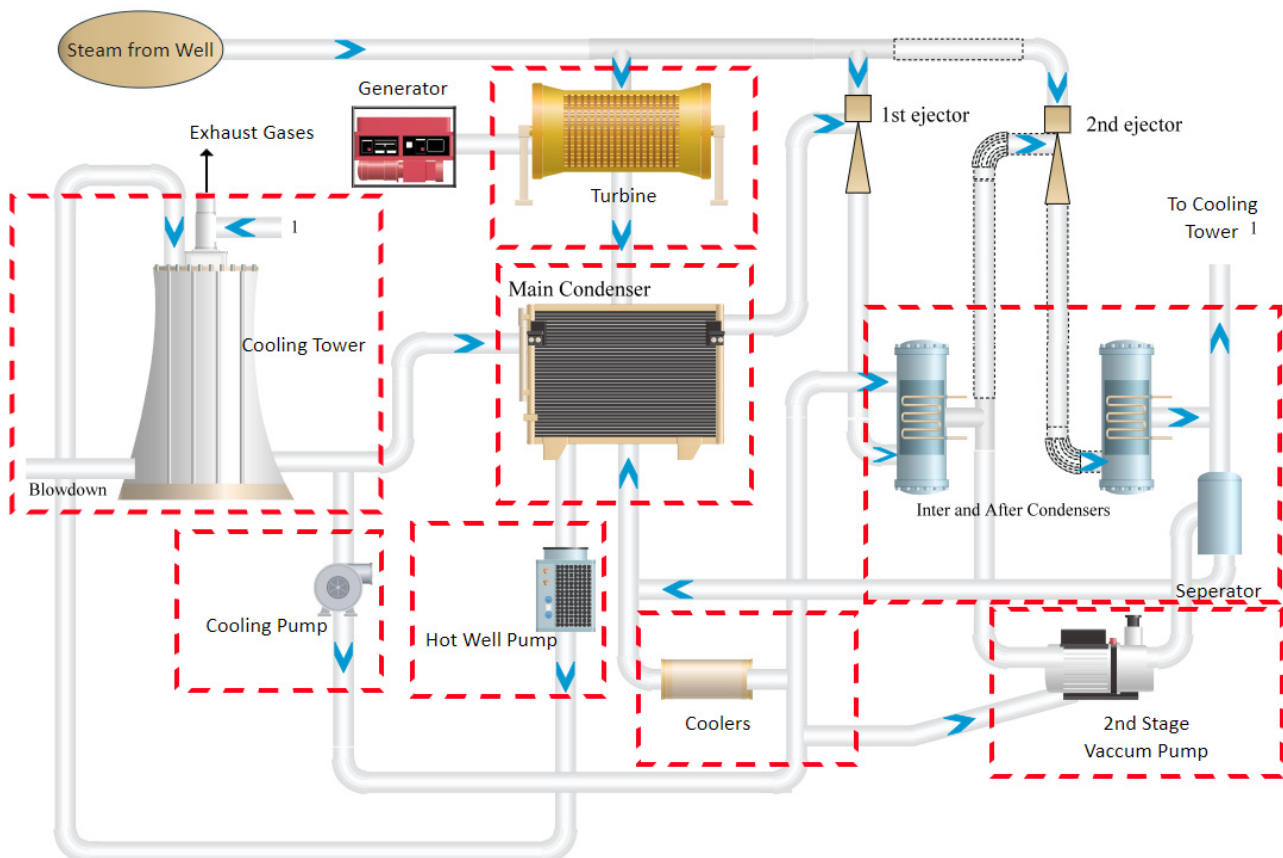


Figure 3. Scope of cost model for conventional geothermal power plant [50].

3. Results and Discussion

This research sought to generate equipment cost correlations according to the QUESTOR modeling and cost database. The reference database was related to the first quarter of 2020, and the extracted correlations were applicable to studies dedicated to future power plant economic assessments. They could help researchers and stakeholders gain a better understanding of the expenses. Comprehensive cost correlations were collected from other research papers and references to compare with the proposed models and understand their reliability. Correlations were generated based on the best compatibility with available data. Different fitting methods were applied to optimize the final results. The obtained results and cost correlations are as follows:

3.1. Compressor

The cost trends for centrifugal and reciprocating compressors are shown in Figures 4 and 5, respectively. In addition to the Turton cost correlation, three other cost correlations were evaluated to compare with the proposed model. Figure 4 shows that the proposed QUESTOR cost model was very close to the Turton, Matche, and Mhhe estimations for carbon steel material, suggesting that these three cost correlations provide better cost estimations than others. The reciprocating compressor's cost trend, based on the proposed model and other cost correlations, is displayed in Figure 5. The closest cost trend to the proposed model was the Turton correlation for carbon steel material.

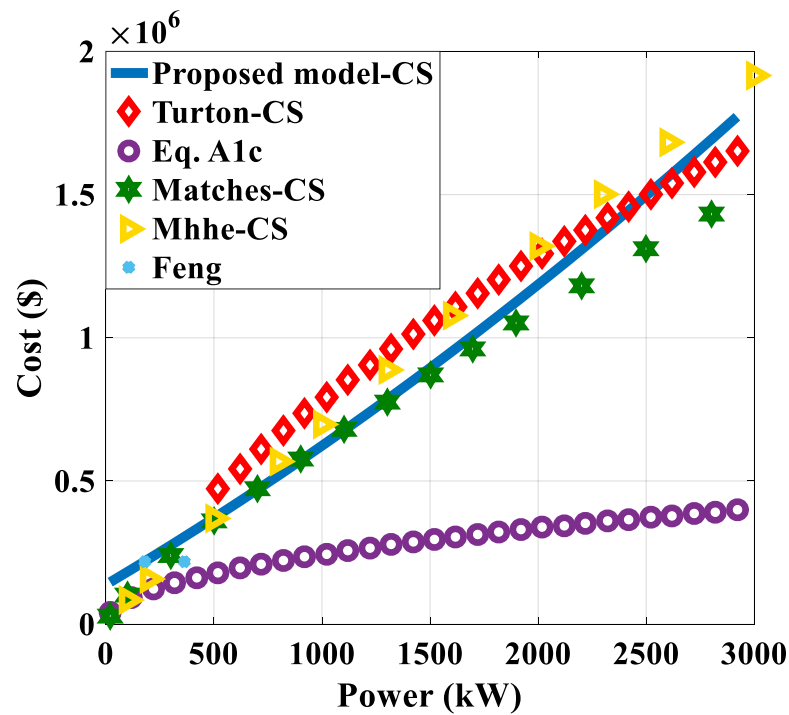


Figure 4. Compressor (centrifugal) cost against power [28,32,48,49,51].

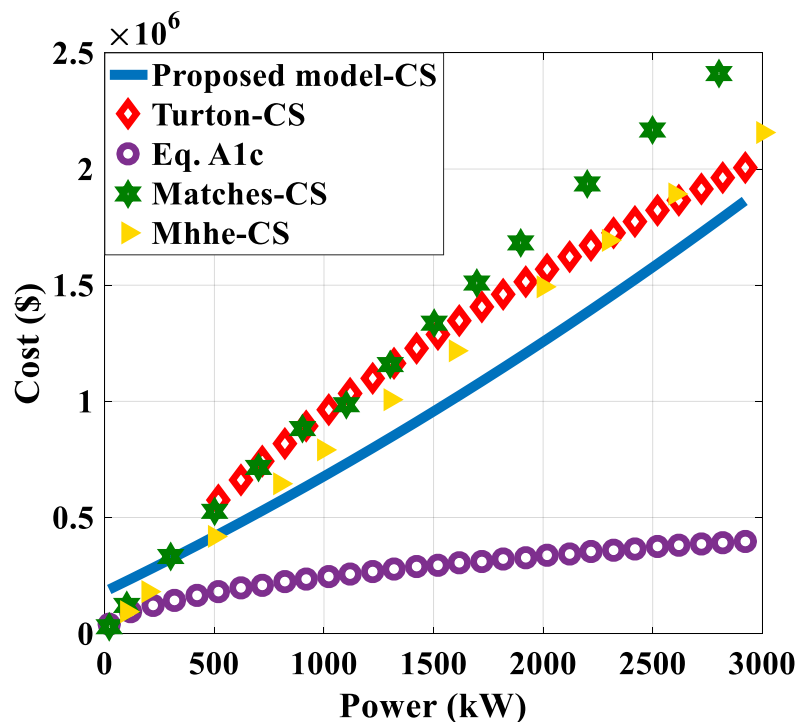


Figure 5. Compressor (reciprocating) cost against power [28,48,49,51].

Moreover, the cost prediction based on Mhhe's and Matche's data was approached that of the proposed QUE\$TOR model. Also, the Feng and Rangaiah [32] presented cost data for low-power compressors fitted with the proposed model. The general form of compressor cost correlation is illustrated in Equation (3), and the coefficients for both compressor types are listed in Table 2.

$$C = \log(\dot{W}_{Comp}) + a.(\dot{W}_{Comp})^2 + b.\dot{W}_{Comp} + c \quad (3)$$

Table 2. The coefficients of Equation (2) for both compressor types.

Compressor Type	<i>a</i>	<i>b</i>	<i>c</i>	<i>R</i> ²
Centrifugal	0.03867	446.7	1.378×10^5	0.99
Reciprocating	0.04147	454.8	1.81×10^5	0.96

In this equation, \dot{W}_{Comp} is compressor power (kW) and *C* is the cost (\$).

3.2. Air Cooler Condenser

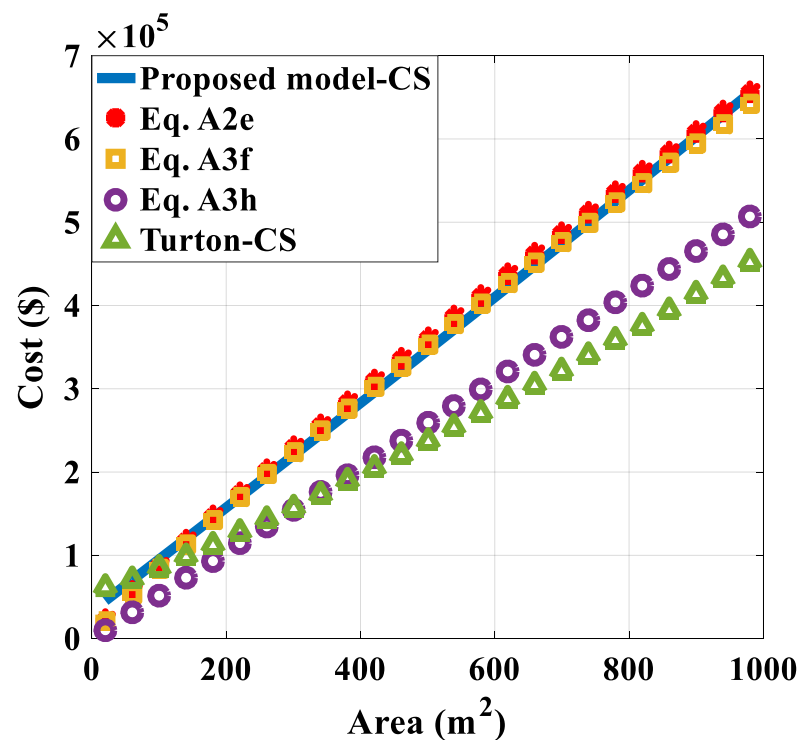
Figure 6 illustrates the air cooler condenser cost trend for the proposed QUESTOR model and other cost correlations. It is clear from this graph that cost trends of Equations (A2e) and (A3f) are compatible with the proposed model; however, the Turton correlation for carbon steel was lower than these correlations. Furthermore, Matche's cost data for air coolers based on different materials are shown in Figure 7. As these costs include stainless steel, it can be seen that they are higher than the proposed model, which is related to carbon steel. The general form of cost correlation for an air cooler is presented in Equation (4), and the relevant correlations are listed in Table 3.

$$C = \log(A) + a.(A)^2 + b.A + c \quad (4)$$

where *A* is compressor power (m²) and *C* is the cost (\$).

Table 3. The coefficients of Equation (3) for air coolers.

Equipment	<i>a</i>	<i>b</i>	<i>c</i>	<i>R</i> ²
Air Cooler	0.01764	617.4	3.31×10^4	0.95

**Figure 6.** Air cooler cost against area [28,52–54].

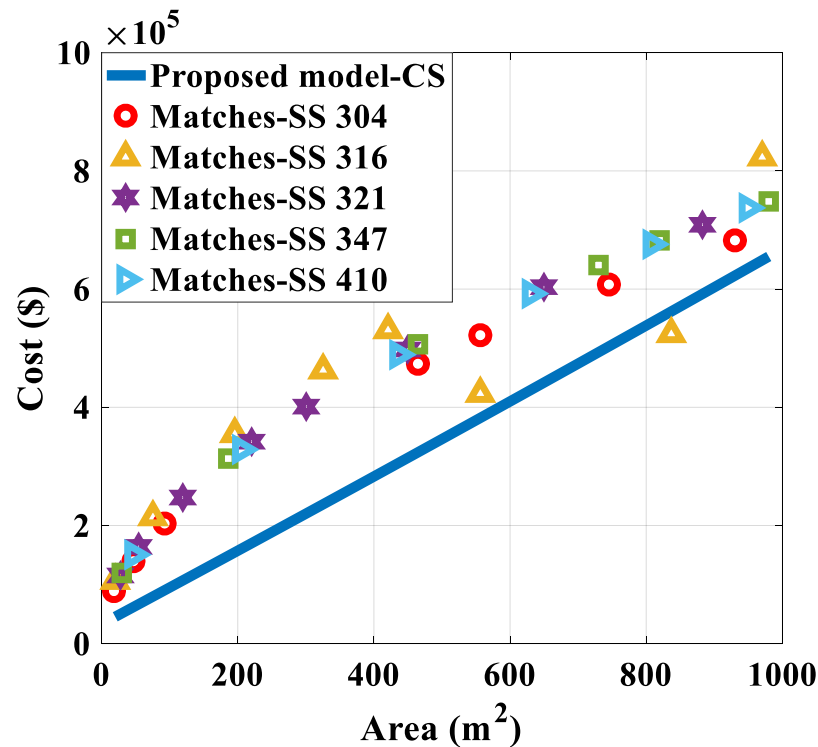


Figure 7. Air cooler cost against area [48].

3.3. Pump

Figure 8 presents cost trends for centrifugal pumps according to the proposed QUE\$TOR model and other cost correlations. Besides the Turton correlations, 14 other pump cost correlations were considered to compare the results with the proposed model. It can be seen that the cost estimation of Equation A4.14 and Turton correlations for carbon steel centrifugal pumps and positive displacement were close to the proposed model. The other cost correlations that are not listed in this graph had an unfitted trend with the presented model. Additionally, the cost data presented by Feng and Rangaiiah [32] for low power pumps were close to the proposed model. The general cost correlation form of pump and corresponding coefficients are presented in Equation (5) and Table 4, respectively.

$$C = \log(\dot{W}_P) + a.(\dot{W}_P)^2 + b.\dot{W}_P + c \quad (5)$$

Table 4. The coefficients of Equation (4) for centrifugal pumps.

Equipment	<i>a</i>	<i>b</i>	<i>c</i>	<i>R</i> ²
Pump	−0.03195	467.2	2.048 × 10 ⁴	0.97

In this equation, \dot{W}_P is compressor power (kW) and *C* is the cost (\$).

3.4. Pressure Vessel

The pressure vessel cost trend for the proposed QUE\$TOR model and other cost correlations are displayed in Figure 9. As can be seen, the cost trend of the Turton correlation for carbon steel pressure vessels was close to the presented model trend for both bullet and sphere types. The Feng and Rangaiiah [32] presented cost data for pressure vessels was acceptably close to the proposed model. The general form of pressure vessel cost correlation based on volume is presented in Equation (6). Also, the relevant coefficients are presented in Table 5.

$$C = \log(V) + a.(V)^2 + b.V + c \quad (6)$$

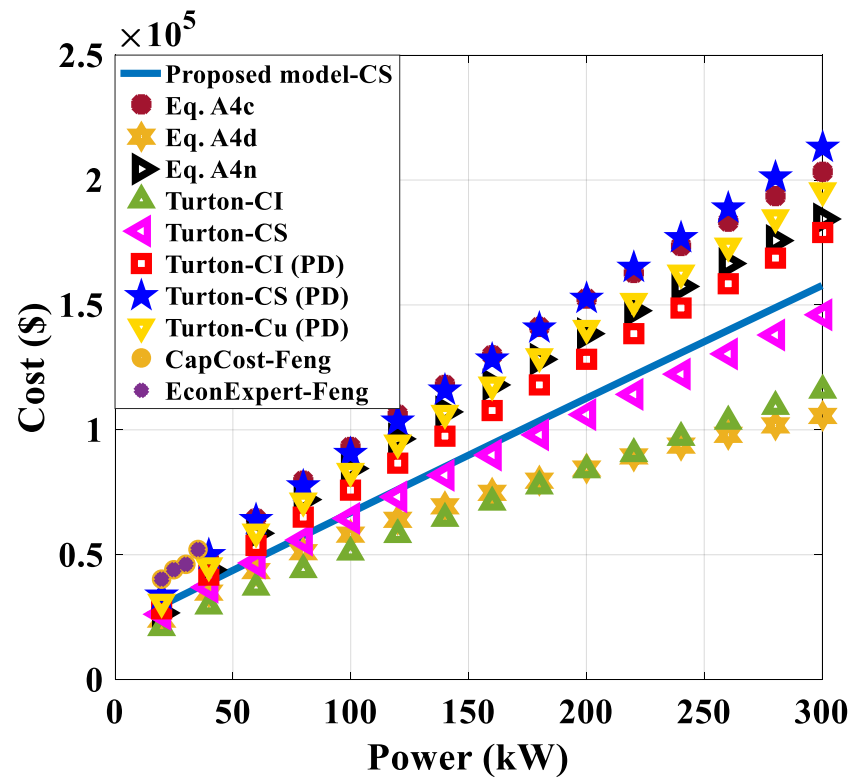


Figure 8. Centrifugal pump cost against power [28,32,55–57].

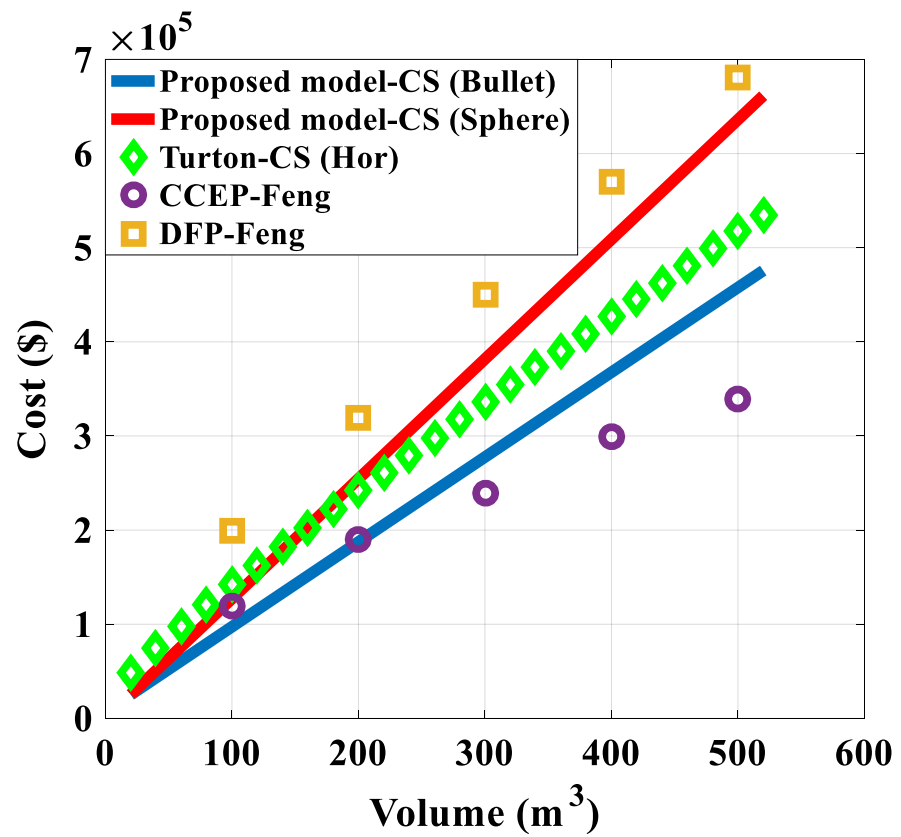


Figure 9. Pressure vessel cost against capacity [28,32].

Table 5. The coefficients of Equation (5) for pressure vessels.

Vessel Type	<i>a</i>	<i>b</i>	<i>c</i>	<i>R</i> ²
Bullet	−0.002745	902.6	7061	0.99
Sphere	−0.001613	1273	−68.46	0.98

Here, *V* is compressor power (m³) and *C* is the cost (\$).

3.5. Heat Exchanger (Shell-and-Tube, Flat Plate)

Figure 10 shows the cost trends for shell-and-tube heat exchangers according to the proposed model and other cost correlations. In addition to the Turton, 33 other heat exchanger cost correlations (presented in Appendix A) were considered in this study. Among these cost correlations, only Equation (A2e) had a trend close to that of the proposed model. As the extracted model was based on a carbon steel shell and stainless steel tube, it can be seen that the Turton cost trend for a U-tube shell-and-tube heat exchanger with carbon steel shell and stainless steel tube was close to the trend obtained with the QUE\$TOR cost model. Figure 11 shows the proposed model and Matche's data and the Feng and Rangaiah [32] data for a shell-and-tube heat exchanger. Feng and Rangaiah [32] presented cost data were related to different programs such as Detailed Factorial Method (DFP), Capital Cost Estimation Program (CCEP), Aspen, CapCost, and Econexpert. The flat plate heat exchanger's cost trend based on the generated QUE\$TOR model and the Turton correlation are displayed in Figure 12. As can be observed, the Turton cost trend for a flat-plate heat exchanger using carbon steel was similar to that of the proposed model, albeit somewhat different. The general form of the generated cost correlation for the heat exchanger is the same for the air cooler based on the area heat exchanger. The corresponding coefficients of cost correlations for both heat exchanger types are presented in Table 6.

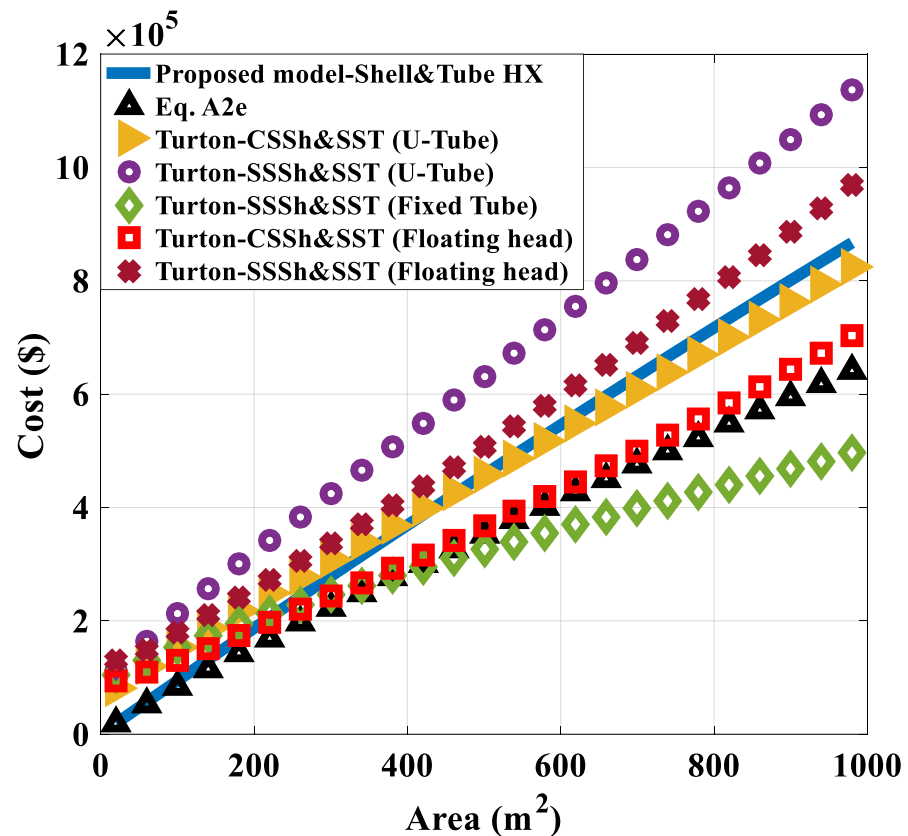


Figure 10. Shell-and-tube heat exchanger cost against the area [28,52].

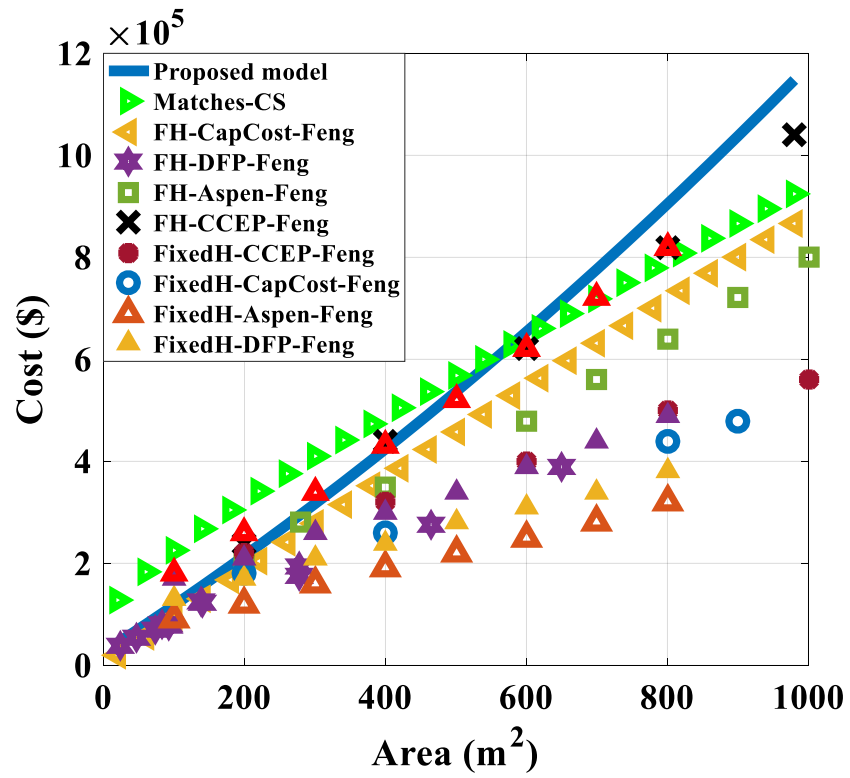


Figure 11. Shell-and-tube heat exchanger cost against the area [32,48].

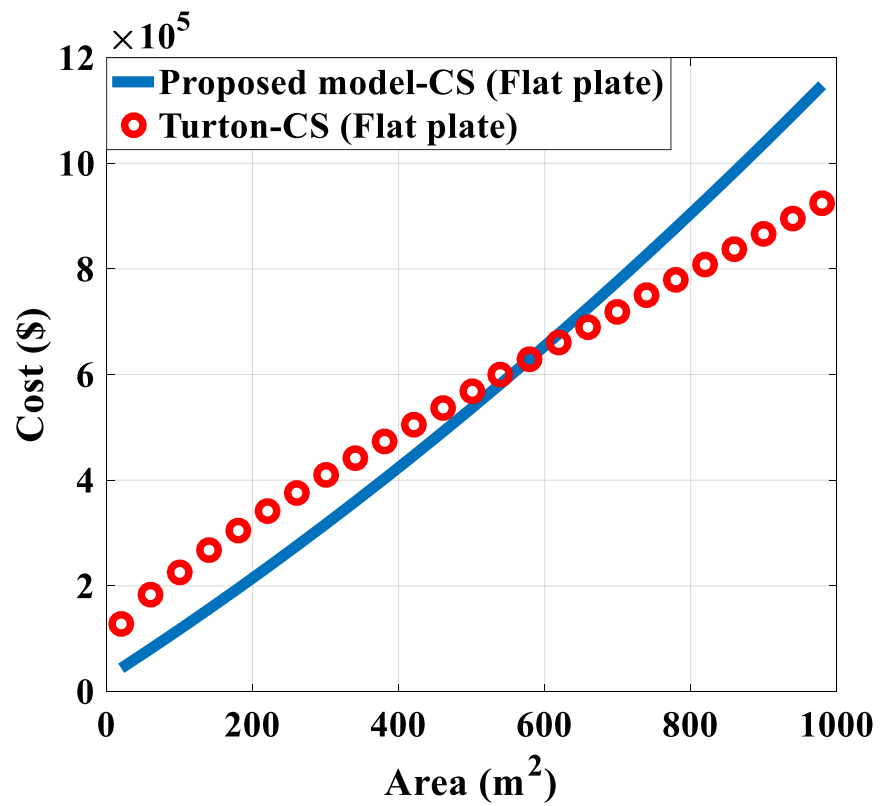


Figure 12. Flat plate heat exchanger cost against area [28].

Table 6. The coefficients of Equation (3) for heat exchangers.

Heat Exchanger Type	<i>a</i>	<i>b</i>	<i>c</i>	<i>R</i> ²
Shell & Tube	−0.06395	947.2	227.9	0.98
Flat plate	0.2581	891.7	2.605×10^4	0.96

The fitting approach in this study was developed by minimizing the residuals to improve the obtained results and equation accuracy. The genetic algorithm was applied to achieve this goal. Some researchers have not applied the optimization method to the cost estimation process, as that could increase the uncertainties and errors of the final models. Other researchers have applied the genetic algorithm optimization approach to calculate the cost correlations with different elements, and all showed promising results compared with other algorithms. However, few research studies have shown consideration for the generation of power plant equipment cost correlations. That is because gathering the equipment cost data is difficult, and the data resources are limited. On the other hand, as other, available studies noted several years ago, these updated and proposed correlations could help researchers and stakeholders to better predict equipment costs.

The proposed models in this study have several advantages compared with earlier models. First, the generated models are related to the 2020 database, which means they are the most recently updated models for the estimation of power plant purchasing costs. These models are suitable for various power cycle cost estimations. Most significantly, the benefit of this work is in applying optimization methods after generating the cost correlations and relevant coefficients. The optimization is done by a genetic algorithm to reduce errors and optimize the cost models based on available data. Other researchers' results have shown that applying optimization methods can reduce the uncertainties of cost estimation. Other studies mainly consider one or two types of equipment when generating their cost correlations; however, in the present work, the most significant equipment cost models are generated in a research package.

4. Conclusions

In this study, the power plant's main equipment costs were considered using QUE\$TOR software, which is linked to cost data for 2020. The considered types of equipment were the pump, compressor, heat exchanger, air cooler, and pressure vessel. The cost data were extracted by modeling in QUE\$TOR and changing the main parameters of the system. After data gathering, the equipment cost correlations based on the available data were generated by applying a robust surface modeling approach. The available cost correlations from different research papers and references were collected to compare the results with the proposed QUE\$TOR model and find better and more reliable correlations. A general form of correlation was generated for each piece of equipment based on its primary dependent variable, and relevant coefficients were calculated based on the best compatibility with available data. Results showed that the Turton correlation and Matche's and Mhhe's cost data for both centrifugal and reciprocating compressors were compatible with the proposed QUE\$TOR model. The proposed cost model related to the air cooler illustrated that Equations (A2e) and (A3f) (presented in Appendix A) had a better fitting than others. Conversely, Equation (A3h) and Turton's cost evaluations for carbon steel were a bit lower than that obtained with the proposed model. Other cost correlations had scattered and unfitted cost trends compared with that of the proposed model. The proposed carbon steel centrifugal pump model showed that Equation (A4n) and Turton carbon steel centrifugal pump cost trends had close results and could calculate reliable cost estimates. Cost correlations for pressure vessels were presented for two different types (bullet and sphere) using carbon steel material. According to the results, the Turton estimation of the pressure vessel for carbon steel and Feng and Rangaiah presented cost had close trends with the proposed models. Based on the obtained results, the Turton cost estimation for shell-and-tube heat

exchangers using carbon steel shell and stainless steel tube had good compatibility with the proposed model.

Moreover, the flat plate cost prediction by Turton for carbon steel flat-plate heat exchanger had a somewhat different trend. The generated cost correlations had high compatibility (about 95%) with the cost data for all evaluated equipment. These correlations were applicable to a wide range of dependent variables (power for pump and compressor, area for heat exchangers, and capacity for pressure vessel). The proposed cost models for all considered equipment are reliable for the evaluation of equipment costs and could help researchers and stakeholders gain a better understanding of the expenses, as these data are updated based on the 2020 database.

Author Contributions: Conceptualization, M.S. and P.H.N.; methodology, M.S.; software, M.S. and P.H.N.; validation, P.H.N. and L.T.; formal analysis, M.S.; investigation, M.S.; data curation, P.H.N. and L.T.; writing—original draft preparation, M.S.; writing—review and editing, P.H.N. and L.T.; supervision, G.M. and D.F.; project administration, G.M. and D.F. All authors have read and agreed to the published version of the manuscript.

Funding: This research received no external funding.

Conflicts of Interest: The authors declare no conflict of interest.

Nomenclature

a, b, c	Coefficients
A	Area, (m ²)
CI	Cast Iron
$CCEP$	Capital Cost Estimation Program
DFP	Detailed Factorial Method
$FixedH$	Fixed head
FH	Floating head
Hor	Horizontal
V	Volume, (m ³)
\dot{W}	Power, (kW)
Z	Capital cost of components, (\$)

Subscripts

$Comp$	Compressor
$Cond$	Condenser
HX	Heat exchanger
P	Pump

Appendix A

Table A1. Compressor purchasing cost equations.

NO	Equation	References
A1a	$Z_{Comp} = 91,562 \times \left(\dot{W}_{Comp} / 455 \right)^{0.67}$	[58]
A1b	$Z_{Comp} = 9624.2 \times \dot{W}_{Comp}^{0.46}$	[59]
A1c	$Z_{Comp} = 10,167.5 \times \dot{W}_{Comp}^{0.46}$	[51]

Table A2. Heat exchanger purchasing cost equations.

NO	Equation	References
A2a	$Z_{HX} = 10,000 + 324 \times A^{0.91}$	[60]
A2b	$Z_{HX} = 130 \times (A/0.093)^{0.78}$	[58]
A2c	$Z_{HX} = 16,000 \times (A/100)^{0.6}$	[58]
A2d	$Z_{HX} = 12,000 \times (A/100)^{0.6}$	[58,61]
A2e	$Z_{HX} = 1397 \times A^{0.89}$	[52]
A2f	$Z_{HX} = 2143 \times A^{0.514}$	[62]
A2g	$Z_{HX} = 2681 \times A^{0.59}$	[63]
A2h	$Z_{HX} = 96.2 \times A$	[64]
A2i	$Z_{HX} = 34.9 \times A$	[64]
A2j	$Z_{HX} = 45.7 \times A$	[64]
A2k	$Z_{HX} = 309.14 \times A^{0.85}$	[65]
A2l	$Z_{HX} = 231.915 + (309.143 \times A)$	[66]
A2m	$Z_{HX} = 190 + (310 \times A)$	[67]
A2n	$Z_{HX} = 588 \times A^{0.80}$	[68]
A2o	$Z_{HX} = 7000 + (360 \times A^{0.85})$	[69]
A2p	$Z_{HX} = 1.3 \times (190 + (310 \times A))$	[70]
A2q	$Z_{HX} = 3.28 \times 10^4 \times (A/80)^{0.68}$	[53]
A2r	$Z_{HX} = 383.5 \times A^{0.65}$	[71]
A2s	$Z_{HX} = 8500 + 409 \times A^{0.85}$	[54]
A2t	$Z_{HX} = 14,000 + 614 \times A^{0.92}$	[72]
A2u	$Z_{HX} = 17,500 + 699 \times A^{0.93}$	[72]
A2v	$Z_{HX} = 885 \times A^{0.432}$	[21]
A2w	$Z_{HX} = 231 \times A^{0.639}$ (flat plate)	[21]
A2x	$Z_{HX} = 1391 \times A^{0.778}$ (flat plate)	[72]
A2y	$Z_{HX} = 635.14 \times A^{0.778}$ (flat plate)	[72]

Table A3. Condenser purchasing cost equations.

NO	Equation	References
A3a	$Z_{Cond} = 8000 \times (A/100)^{0.60}$	[55,58,61]
A3b	$Z_{Cond} = 516.62 \times A^{0.60}$	[56]
A3c	$Z_{Cond} = 2143 \times A^{0.514}$	[63]
A3d	$Z_{Cond} = 8500 + 406 \times A^{0.80}$	[66]
A3e	$Z_{Cond} = 297 \times A$	[67]
A3f	$Z_{Cond} = 1.56 \times 10^5 \times (A/200)^{0.89}$	[53]
A3g	$Z_{Cond} = 2382.9 \times A^{0.68}$	[51]
A3h	$Z_{Cond} = 516.621 \times A + 268.45$	[54]

Table A4. Pump purchasing cost equations.

NO	Equation	References
A4a	$Z_p = 705.48 \times \dot{W}_p^{0.71} (1 + (0.2/1 - \eta_p))$	[73]
A4b	$Z_p = 2100 \times (\dot{W}_p/10)^{0.26} (1 - \eta_p/\eta_p)^{0.5}$	[58,61]
A4c	$Z_p = 3540 \times \dot{W}_p^{0.71}$	[55,74]
A4d	$Z_p = 200 \times \dot{W}_p^{0.65}$	[56,60,65]
A4e	$Z_p = 1120 \times \dot{W}_p^{0.80}$	[63,75]
A4f	$Z_p = 549.13 \times \dot{W}_p^{0.71} \times 1.41 \times (1 + (0.2/1 - \eta_p))$	[64]
A4g	$Z_p = 900 \times (\dot{W}_p/300)^{0.25}$	[67]
A4h	$Z_p = 500 \times (\dot{W}_p/300)^{0.25}$	[67]
A4i	$Z_p = 16,800 \times (\dot{W}_p/200)^{0.67}$	[76]
A4j	$Z_p = 1000 \times \dot{W}_p^{0.65}$	[55]
A4k	$Z_p = 1785 \times (\dot{W}_p/1000)^{0.71} (1 + (0.2/1 - \eta_p))$	[77]
A4l	$Z_p = 3500 \times \dot{W}_p^{0.41}$	[78]
A4m	$Z_p = 9.84 \times 10^3 (\dot{W}_p/4000)^{0.55}$	[53]
A4n	$Z_p = 3 \times 422 \times \dot{W}_p^{0.71} \times 1.41 \times (1 + (0.2/1 - \eta_p))$	[57]

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