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Large-eddy simulation of n-dodecane spray flame: Effects of nozzle diameters on autoignition at varying ambient temperatures

Jiun Cai Ong^a, Kar Mun Pang^{b,*}, Xue-Song Bai^c, Mehdi Jangi^d, Jens Honore Walther^{a,e}

^aDepartment of Mechanical Engineering, Technical University of Denmark, 2800 Kgs. Lyngby, Denmark
^bMAN Energy Solutions, 2450 København, Denmark
^cDepartment of Energy Sciences, Lund University, 22100 Lund, Sweden
^dDepartment of Mechanical Engineering, University of Birmingham, Birmingham, B15 2TT, UK
^eComputational Science and Engineering Laboratory, ETH Zürich, CH-8092 Zürich, Switzerland

Abstract

In the present study, large-eddy simulations (LES) are used to identify the underlying mechanism that governs the ignition phenomena of spray flames from different nozzle diameters when ambient temperature (T_{am}) varies. Two nozzle sizes of 90 μ m and 186 μ m are chosen. They correspond to the nozzle sizes used by Spray A and Spray D, respectively, in the Engine Combustion Network. LES studies of both nozzles are performed at three T_{am} of 800K, 900K and 1000K. The numerical models are validated using the experimental liquid and vapour penetration, mixture fraction (Z) distribution, as well as ignition delay time (IDT). The ignition characteristics of both Spray A and Spray D are well predicted, with a maximum relative difference of 14% as compared to the experiments. The simulations also predict the annular ignition sites for Spray D at $T_{am} \ge 900$ K, which is consistent with experimental observation. It is found that the mixture with $Z \le 0.2$ at the spray periphery is more favorable for ignition to occur than the overly fuel-rich mixture of Z > 0.2 formed in the core of spray. This leads to the annular ignition rates (χ) during high temperature ignition. The maximum χ during high temperature ignition for Spray D is larger than that in Spray A by approximately a factor of 5. In contrast, at $T_{am} = 1000$ K, the χ values are similar between Spray A and Spray D. This elucidates the increase in the difference of IDT between Spray D and Spray A as T_{am} decreases. This also explains the contradicting findings on the effects of nozzle diameters on IDT from literature.

Keywords:

Spray A, Spray D, Autoignition, Nozzle Size, LES

^{*}Corresponding author: Kar Mun Pang

Email address: kar.pang@man-es.com (Kar Mun Pang)

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1. Introduction

Understanding the ignition characteristics of diesel spray combustion is critical as a longer ignition delay time (IDT) increases the local pre-combustion mixing, thus reducing emission [1, 2]. Different nozzle diameter sizes (D_{noz}) show significant effect on the ignition characteristics in diesel engines [3–7]. Decreasing D_{noz} was shown to reduce the IDT [3, 7]. At the same time, other studies [4-6] showed contradicting findings, where varying the D_{noz} had no significant effects on the IDT in a diesel engine. It is worth mentioning that incylinder flow varies from one engine to another due to different piston bowl and intake valves configurations. The injection characteristics were also not standardized. Hence, the air-fuel mixing is expected to vary as well. These collectively make direct comparison of the results from different diesel engine data difficult.

To better understand the effect of D_{noz} on ignition characteristics without the complex in-cylinder flow, experimental studies were carried out in a constant volume vessel with controlled ambient pressure and temperature conditions which resemble those of direct injection diesel engines. One of the earliest works on investigating different D_{noz} for diesel spray combustion was carried out by Sieber and Higgins [8, 9] using the grade number two diesel fuel (diesel #2). IDTs from four D_{noz} of 100 μ m, 180 μ m, 246 μ m and 363 μ m at varying ambient temperatures (T_{am}) from 800K–1200K are available on ECN [9]. This work focused on the effects of D_{noz} on flame stabilization. Revisiting the associated IDTs in the study reveals a non-monotonic trend when D_{noz} varies. At $T_{\text{am}} \ge 900K$, varying $D_{\rm noz}$ have no significant effect on IDT. However, at 800K, the IDTs exhibit a non-monotonic trend where $IDT_{180\mu m}$ < $IDT_{100\mu m}$ < $IDT_{246\mu m}$. Thereafter, a great amount of experimental and numerical effort was placed in studying Spray A in the Engine Combustion Network (ECN) [9], which uses *n*-dodecane fuel $(C_{12}H_{26})$ and a D_{noz} of 90 μ m. The baseline ambient conditions are standardized to a $T_{\rm am}$ of 900K, gas density ($\rho_{\rm am}$) of 22.8kg/m³, and molar oxygen concentration (O_{2.am}) of 15%.

Recently, Spray D configuration is introduced by ECN, which has the same ambient conditions and fuel type as Spray A, but uses an injector that has approximately twice the size of the nominal D_{noz} of Spray A. Experimental studies on ignition and combustion characteristics of Spray D were performed by Westlye [10] and Pastor et al. [11]. The IDT measurement of Spray A and Spray D took into account the hydraulic delay during fuel injection and were

based on natural luminosity from the flame. Different $T_{\rm am}$, $O_{2,\rm am}$ and injection pressures $(P_{\rm inj})$ were varied in their experimental studies. Spray D was shown to have a longer IDT than Spray A across different $T_{\rm am}$ [11]. The slower mixing in Spray D was suggested to be the main reason for this observation [11]. The experimental studies also showed that the differences in IDTs between Spray D and Spray A were increasing as $T_{\rm am}$ decreases. The physics behind this was, however, not clearly addressed in the paper.

From a simulation point of view, Pang et al. [12] performed a three-dimensional, computational fluid dynamics (CFD) study on reacting sprays in a constant volume combustion vessel with D_{noz} of 100 μ m, 180 μ m and $363\mu m$. The simulations were carried out by coupling unsteady Reynolds-averaged Navier-Stokes with an Eulerian Stochastic Field method [12]. Their results were consistent with experimental observation, which showed no significant effect on IDT across the three D_{noz} at T_{am} of 1000K. Comparison of Spray D and Spray A was carried out in the numerical study by Desantes et al. [13]. It was shown that a reduction in $D_{\rm noz}$ promotes faster mixing which shortens the time needed to reach ignitable equivalence ratio, therefore shorter IDT. All the numerical works mentioned above for different D_{noz} were only performed at a single T_{am} . On the other hand, comprehensive studies of the effects of $T_{\rm am}$ on ignition and spray flame were carried out by Pei et al. [14] and Pang et al. [15]. However, the works were carried out only for small D_{noz} . Therefore, the coupled effects between D_{noz} and T_{am} on ignition characteristics are still not well understood.

Set against these backgrounds, this paper first aims to identify the underlying mechanism that controls the ignition process of spray flame from different D_{noz} at varying T_{am} . Further emphasis is placed on understanding the experimentally observed increasing difference of IDTs between Spray D and Spray A as T_{am} decreases. Moreover, this work also aims to resolve the contradicting findings on the effects of D_{noz} on IDT from literature. These aims are achieved by performing large-eddy simulations (LES) of Spray A and Spray D at T_{am} of 800K, 900K, and 1000K.

2. Numerical methods and case setup

The present LES is performed using OpenFOAMv1712. Eulerian-Lagrangian approach is used within the LES framework for spray modelling. The gas phase is described using spatially filtered transport equations. Both temporal and spatial terms are discretized using implicit second-order schemes. The sub-grid scale (SGS) is modeled using the Dynamic *k*-equation. The pressure-velocity coupling is implemented in terms of the Pressure Implicit with Splitting of Operator (PISO) algorithm. The injected liquid phase of $C_{12}H_{26}$ is modeled as discrete parcels whose motion is described using the Lagrangian particle tracking approach. Each parcel represents a group of spherical droplets whose position, size, and physical properties are similar. Fuel droplet breakup is modeled by the Reitz-Diwakar model, where the stripping break up constant, C_s is set to 10 [16]. The Frossling model and the Ranz-Marshall correlation are employed to account for the droplet evaporation and heat transfer with the surrounding gas phase, respectively.

The skeletal C12H26 mechanism developed by Yao et al. [17] (54 species and 269 reactions) is used in this work. The mechanism has shown good performance in spray combustion context [18, 19]. The partially stirred reactor (PaSR) [20] combustion model is used to account for the turbulence-chemistry interactions, where the C_{mix} is set to 0.3. The Chemistry Coordinate Mapping (CCM) approach is coupled with the PaSR combustion model in order to speed up the integration process of the chemical reaction rates [21]. This method has been successfully implemented to LES of spray combustion [22]. The current work uses a fourdimensional phase space based on temperature, local equivalence ratio, scalar dissipation rate, and the mass fraction of fuel, where the CCM resolutions are fixed at 5K, 0.01, 0.025, and 0.001, respectively [15, 21].

The experimental reference case for the simulations in the current study corresponds to ECN Spray A $(D_{\text{noz}} = 90\mu\text{m})$ and Spray D $(D_{\text{noz}} = 186\mu\text{m})$ baseline conditions [9]. Both Spray A and Spray D have the same P_{inj} of 1500bar, fuel temperature of 363K and ρ_{am} of 22.8kg/m³. The operating conditions and the fuel injection are summarized in Table 1, where \dot{m}_f denotes the injected fuel mass flow rate. Cases 1–4 are Spray A cases; while cases 5-8 are Spray D cases. Cases 1 and 5 are inert spray cases, where the $O_{2,am}$ is set to zero. The ambient mixture composition and temperature are initiated as uniform field while the velocity field is set to zero. Details of the ambient composition can be found in [9]. The computational domain is a constant volume cubic chamber with side lengths of 108mm. All boundaries are set as no-slip, adiabatic wall. The injector is placed at the center of one of the chamber walls. A uniform mesh of 0.125mm is used within the spray combustion region (80mm axially and 15mm radially from the nozzle location) and a coarser mesh resolution is used outside the spray combustion region. This mesh resolution is the same as those reported in

Table 1: Operating	conditions and injector	specifications
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Case	$O_{2,am}$	$T_{\rm am}$	$D_{\rm noz}$	\dot{m}_f
	[% mol]	[K]	[µm]	[mg/ms]
1	0	900	90	2.295
2	15	800	90	2.295
3	15	900	90	2.295
4	15	1000	90	2.295
5	0	900	186	11.71
6	15	800	186	11.71
7	15	900	186	11.71
8	15	1000	186	11.71

[14, 23]. The current setup is shown in Section 3 to accurately capture the penetration lengths, mixture fraction profiles and IDT.

3. Validation of models

3.1. Inert spray

While validation of LES using Spray A data can be widely found in the literature, those using Spray D are scarcely found to the best of the authors' knowledge. The validation of the computational setup is carried out by comparing the liquid penetration length (LPL), vapour penetration length (VPL) and the radial mixture fraction profiles at two axial positions with the experimental data of ECN [9]. LPL is defined as the maximum axial location from the injector to the location where 95% of the total liquid mass is found; VPL is determined using the farthest downstream location of 0.1% fuel mass fraction.

Figure 1a shows the comparison of simulated LPL and VPL against measurements data. It is important to note that the same numerical configurations are used in both Spray A and Spray D simulations. Without calibrating any other model constant for each spray, the penetration lengths predicted for Spray A and Spray D are in good agreement with experimental data.

In addition, mixture fraction (Z) fields of Spray A and Spray D are compared with experimental data in Figure 1b in normalized radial (r^*) and axial (x^*) coordinates. The radial coordinate (r) and axial coordinate (x) are normalized by the equivalent diameter (d_{eq}) of each nozzle, i.e., $r^* = r/d_{eq}$ and $x^* = x/d_{eq}$ [11, 13]. The equivalent diameter is calculated as $d_{eq} = D_{noz} \sqrt{\rho_f / \rho_{am}}$, where ρ_f denotes the density of fuel. It is also shown in [11, 13] that the Z profiles for Spray A and Spray D collapse onto one another in normalized coordinates. It is hence possible to compare the Z fields for Spray A and Spray D against the experimental data for Spray A. The Z profiles are obtained from a single LES realization by time averaging from 1.5 to 2ms. An additional spatial averaging is performed in the circumferential direction. As shown in Figure 1b, the model shows good qualitative agreement for both Spray A and Spray D at $x^* = 35$ and 50 for $|r^*| \ge 2$. The underprediction close to the spray centerline can be improved by increasing the spatial resolution [24] but at a much higher computational cost. Considering that the current computational setup achieves a balance between accuracy and computational efficiency, the same setup is used next in simulating the reacting spray cases.



Figure 1: (a) Penetration lengths of liquid and vapour fuel for Spray A (solid-lines) and Spray D (dashed-lines). (b) Average mixture fraction distribution along normalized radial direction, r^* at normalized axial distance, $x^* = 35$ and 50. The gray shadow represents the error bar of 95% confidence interval for the measurements.

3.2. Reacting spray

In the following analysis, the IDTs for Spray A and Spray D at different T_{am} are simulated and compared against measurement data, as shown in Figure 2a. The computed IDTs have the same definition as the measurement data, which is the time from start of injection to the time when the maximum rate of maximum temperature rise in the domain occurs [14]. This definition is in accordance to ECN recommendation [9]. From Figure 2a, the predicted

IDTs across different temperatures has a maximum relative difference of 14% compared to measurements. Furthermore, the predicted IDT for Spray D is shown to be longer than Spray A across the three $T_{\rm am}$, where the largest deviation is at 800K. This observation corresponds to the findings in [11].

Further validation is performed to assess the model performance in predicting intermediate species. The instantaneous mass fraction distributions of important intermediate combustion product, such as formaldehyde (CH₂O) and hydroxide (OH) at IDT for Spray A at $T_{\rm am} = 900$ K are compared against measurement data obtained from planar laser induced fluorescence (PLIF) [9, 25]. It can be seen from Figure 2b that a good qualitative agreement between LES and measurements is obtained for the spatial distribution of CH₂O and OH.



Figure 2: (a) The IDTs for the LES cases at different T_{am} . Solid lines - Measurement; Dotted lines - Simulation. Filled symbols - Spray A; Hollow symbols - Spray D. (b) Comparison of CH₂O and OH distributions from PLIF measurements [9, 25] (top) and LES calculations (bottom) at IDT for Spray A at T_{am} = 900K. Spatial units in mm.

4. Results and discussion

In this section, the ignition characteristics obtained from LES of Spray A and Spray D at T_{am} of 1000K and 800K are investigated and compared. For all four cases (Case 2, 4, 6 and 8 in Table 1), the 1st-stage ignition first initiates in fuel-lean region ($Z < Z_{st}$), where Z_{st} is the stoichiometric mixture fraction with a value of 0.045 [14]. It is followed by an apparent temperature rise within the fuel-rich region $(Z > Z_{st})$. Thereafter, the high temperature combustion occurs within a relatively less-rich mixture. These observations agree with the findings by Pei et al. [14]. However, the associated spatial distribution of intermediate species (e.g. CH₂O) as well as ignition location are different between Spray A and Spray D. Moreover, mass fraction of dodecyl peroxide radicals, C12H25O2 (RO2 is henceforth used for brevity) is often used as an indicator for the 1ststage ignition activity [26] as it is one of the important species in the decomposition pathway of *n*-dodecane fuel. Therefore, the spatial distributions of both RO₂ and CH₂O are considered in the following analysis.

4.1. Ignition characteristics at high T_{am} ($T_{am} = 1000K$)

Figure 3 illustrates the temporal evolution of reacting spray at 1000K for Spray A (Figure 3a-c) and Spray D (Figure 3d-f). At 0.18ms (after the 1st-stage ignition occurs), a significant amount of CH₂O is observed downstream (x > 10mm) of Spray A, while significant amount of RO2 is only present at the upstream region just after the liquid spray (cf. Figure 3a). At 0.22ms, the concentration of CH₂O at the head of the spray has decreased, while high concentration of CH₂O remains upstream of the spray, at the end of the liquid spray. From 0.22ms to 0.28ms, Figure 3b depicts that the reacting spray tip region of Spray A has multiple ignition sites ($\Delta T > 400$ K). These igntion sites subsequently spread to the whole spray head as shown in Figure 3c. This location coincides with the ignition region observed experimentally in [9]. Furthermore, the predicted ignition sites occur in regions where the scalar dissipation rates, X, are less than $10s^{-1}$, which agrees well with the findings in [27].

On the other hand, Spray D exhibits a different ignition characteristics than in Spray A. At 0.18ms, RO₂ and CH₂O coexist in the spray head region as shown in Figure 3d. The high concentration of RO₂ at the spray head indicates that the fuel is decomposing to RO₂. At subsequent time (t = 0.22ms), most of the RO₂ has decomposed into intermediate species, such as CH₂O. Hence, a high concentration of CH₂O is present downstream of the spray, while RO₂ is only present upstream of the spray. At 0.22ms, the χ values at both the spray head (indicated by black arrow) and peripheral region (indicated by red arrows) are equally low (< 10s⁻¹), as shown in Figure 3e. It is also worth mentioning that the local temperature in both

regions are approximately 1400K. However, only the mixture at the peripheral of the spray undergoes high temperature ignition (cf. Figure 3f). This can be explained by examining the mixture fractions, Z at both locations. The spray center region (x > 30mm) has a fuel-rich mixture of Z > 0.2. In contrast, the peripheral of the spray, where high temperature ignition occurs, has a mixture of $Z \leq 0.2$. It indicates that overly fuel-rich (Z > 0.2) regions are unfavorable for ignition despite having low X and a temperature of approximately 400K above T_{am} . Hence, the peripheral of the spray, which has a low X value and $Z \leq 0.2$, becomes the most favorable location for ignition. The ignition at the spray periphery is consistent with the experimental observation in [11] where the broadband



Figure 3: The temporal evolution of RO₂, CH₂O and ΔT fields at 1000K for Spray A (a–c) and Spray D (d–f). ΔT defined as the change of temperature relative to $T_{\rm am}$. The stoichiometric mixture fraction, $Z_{\rm st}$ is shown by a gray solid line. The scalar dissipative rates, χ of 10s⁻¹ and 1s⁻¹ are represented by red solid line and black solid line, respectively. Solid magenta line indicates the averaged liquid length. The range considered for the iso-surface of RO₂ is 1×10^{-4} and 5×10^{-3} ; for CH₂O is 6×10^{-3} and 16×10^{-3} ; and for ΔT to be 400K and 1200K. Red arrow indicates high temperature ignition. Black arrow indicates no ignition. For a–c, each frame above shows 15mm × 30mm; whereas for d–f, each frame above shows 20mm × 40mm.

luminosity measured for Spray D at T_{am} of 900K shows an annular ignition site with high concentration of OH radicals. This observation implies that the active locations for ignition are at the spray peripheral. It is worth mentioning that the high temperature regions from the spray periphery converge at the spray head at approximately 0.1ms after IDT.

4.2. Ignition characteristics at low T_{am} ($T_{am} = 800K$)

The ignition characteristics for low T_{am} are illustrated in Figure 4. For Spray A in particular, some similarities in the temporal evolution of reacting spray can be observed between the 800K and 1000K case. Before 1.0ms (not shown), a small amount of RO_2 is initially formed at the spray head (indicated by the blue arrow in Figure 4a) and the ignition kernels subsequently propagate to the whole frontal region of the spray. As such, high concentration of CH₂O is seen at the spray head in Figure 4a at 1.0ms. Meawhile, regions of $\Delta T >$ 400K starts to appear at the tip of the spray head where the local X value is less than $1s^{-1}$. It is noteworthy that the X value is an order of magnitude lower than that in the 1000K case. In subsequent time frames (Figure 4b and c), the high temperature region starts to propagate throughout the spray head and a higher temperature is attained. This trend is similarly obtained in [27] for Spray A at $T_{am} = 750$ K.

The ignition phenomenon of Spray D is different from Spray A, as depicted in Figure 4d-f. At 1.0ms (not shown), the onset location of the 1st-stage ignition for Spray D occurs at the spray periphary (indicated by the blue arrow in Figure 4d) but not at the spray head as in Spray A. Furthermore, the 1st-stage ignition takes place in the vicinity of the spray core region where the cold, fuel-rich mixture prohibits ignition to occur. Hence, the ignition kernel can only propagate downstream along the side of the spray as shown in Figure 4d (t = 1.0ms). At this time instance, the formation of CH₂O occurs at the side of the spray, but not at the spray head. Only until 1.1ms, a significant amount of CH₂O and RO₂ are present at the spray head as shown in Figure 4e. Meanwhile, ignition sites where $\Delta T > 400$ K start to form at the peripheral of the spray and slowly propagate toward the center region. As more ignition sites are formed at the side of the spray and even at the spray head, a volumetric ignition process can be observed in Figure 4f. One should note that the annular ignition pattern seen in the previous section is not observed in this low T_{am} case. This implies that the annular pattern is only profound at high T_{am} where the associated chemical time scale is shorter and the ignition sites fall closer to the liquid fuel.



Figure 4: The temporal evolution of RO₂, CH₂O and ΔT fields at 800K for Spray A (a–c) and Spray D (d–f). The scalar dissipative rates, χ of 1s⁻¹ and 0.1s⁻¹ are represented by red solid line and black solid line, respectively. The range considered for the iso-surface of CH₂O is 3×10^{-3} and 16×10^{-3} . Other information and descriptions can be found in the caption of Figure 3. Blue arrow indicates 1st-stage ignition. For a–c, each frame above shows 25mm × 50mm; whereas for d–f, each frame above shows 40mm × 80mm.

It is worth mentioning that Spray D takes a longer time to achieve high temperature ignition than Spray A for the same time instances (cf. Figure 4). This can be attributed to the difference in χ between Spray D and Spray A. Figure 5 shows the scatter plot of OH and χ for Spray A and Spray D at their respective IDTs. At 800K, the maximum χ in Spray D is higher than in Spray A by approximately a factor of 5. A high χ leads to longer IDT [28], hence explaining the longer IDT obtained in Spray D than in Spray A. On the other hand, at 1000K, the OH- χ distribution of Spray A and Spray D coincides with each other. Thus, indicating that the IDT for 1000K case will be more of less the same. This result corresponds with the observation in Section 3 and experiment [11], which shows that the difference of IDT between Spray D and Spray A increases as T_{am} decreases.



Figure 5: Scatter plots of mass fraction of OH and scalar dissipation rates, χ for Spray A and Spray D at their respective IDTs. Top: $T_{am} = 800$ K. Bottom: $T_{am} = 1000$ K.

5. Conclusion

The present work implements LES with a finiterate chemistry to study the coupled effects of $T_{\rm am}$ and $D_{\rm noz}$. The LES model captures the key characteristics of different $D_{\rm noz}$ of 90 μ m (Spray A) and 186 μ m (Spray D) at three $T_{\rm am}$ of 800K, 900K and 1000K. The liquid penetration length, vapour penetration length and radial mixture fraction profiles are well predicted as compared to experimental data. Furthermore, IDTs at different $T_{\rm am}$ for Spray A and Spray D are captured with a maximum relative difference of 14% as compared to measurements.

At $T_{\rm am} = 1000$ K, both experiment and LES show comparable IDTs between Spray A and Spray D. The numerical results show that the X and thermochemical conditions prior to high temperature ignition are both similar. The local Z, however, strongly influences the ignition pattern. The high temperature ignition site for Spray A occurs at the spray head, whereas it occurs at the peripheral of the spray in Spray D. The ignition process in Spray D leads to an annular ignition pattern, which was demonstrated experimentally and replicated in the present LES study. Despite having a maximum temperature of 400K above $T_{\rm am}$ at the center region of the spray head, the current result suggests that the mixture is unfavorable for ignition due to having fuelricher mixture (Z > 0.2). Instead, the ignition occurs at the peripheral of the spray where $Z \leq 0.2$. The annular pattern of ignition sites is observed at $T_{am} \ge 900$ K, where the associated chemical time scale is shorter and the ignition sites fall closer to the liquid fuel.

At $T_{am} = 800$ K, the IDT is longer for Spray D, which is replicated in the LES. While the thermochemical conditions are similar in these two cases, the maximum χ for Spray D is higher than that in Spray A by approximately a factor of 5. The lower χ is found to be the main factor that leads to the larger difference in IDT between Spray A and Spray D. It is also noted that the χ values at 800K are an order of magnitude lower than those at 1000K, regardless of D_{noz} .

This work explains the increase in the difference of IDT between Spray D and Spray A as T_{am} decreases, which also shed light on the contradicting results from literature.

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